



Several preliminary communications have described anionic polymerizations in DMSO<sup>10-12</sup> and this paper gives details of the polymerization of ethylene oxide initiated by potassium tert-butoxide.

## EXPERIMENTAL

*Materials*

*Dimethyl sulphoxide*—Dimethyl sulphoxide (Guest Industries Ltd, industrial grade) was distilled in an all glass apparatus under nitrogen at reduced pressure. The first fraction, of boiling point up to 106°C at 18–20 mm Hg, was discarded. The middle fraction (b.pt 106°C–107°C at 18–20 mm Hg) was retained and stirred over freshly powdered barium oxide for two days. The supernatant liquid was decanted on to freshly powdered barium oxide and distilled at a controlling reduced pressure (6–7 mm) under dry nitrogen using a five foot column packed with Fenske helices. The fractions collected had a boiling point of 65°–66°C at 6 mm Hg, and were stored in sealed vessels containing fresh barium oxide. As required these vessels were joined to flasks via the break-seal and attached to the vacuum line. After breaking the seal of the original flask, by means of a metal-in-glass breaker used in conjunction with a magnet, and degassing by the usual freezing–melting technique, molecular distillation under high vacuum conditions was carried out. The receiver was cooled in liquid nitrogen and the flask containing the dimethyl sulphoxide was warmed in warm water (60°–70°C). The final pure dimethyl sulphoxide was used as required, and was never opened to air.

Various other purification techniques were tried. Distillation from the initiator to be used, potassium tert-butoxide, was one such process. Another was employing calcium hydride as the drying agent. Both of these techniques failed to improve upon the purity of the dimethyl sulphoxide. The former may possibly introduce tert-butanol into the system, while the latter contains calcium carbide as an impurity which will react with any water present forming acetylene. As dimethyl sulphoxide is one of the best known solvents for acetylene this might seriously affect an anionic polymerization reaction.

*Potassium tert-butoxide*—Crude potassium tert-butoxide (ca. 25 g) was pumped for about 24 hours under high vacuum conditions while at a temperature of 80°–90°C maintained by a water bath. This removed all the tert-butyl alcohol except that associated with the alkoxide as alcohol of crystallization. The bulk of this product was retained in a stoppered vessel until needed.

As required portions of the potassium tert-butoxide (ca. 3–4 g) were sublimed in a vacuum sublimation apparatus at 160°C under high vacuum conditions. The cold finger was maintained at 0°C by means of ice-water. The pure product was stored in sealed glass phials under vacuum until required.

*Ethylene oxide*—Ethylene oxide (B.D.H. Laboratory reagent) was distilled, under high vacuum at 0°C, after degassing, on to calcium hydride in a flask fitted with a greased vacuum tap. This stock solution was retained in the refrigerator and as required aliquots were distilled from this flask under high vacuum at 0°C.

*Solvents*—All solvents and other reagents were analytical reagent grade materials used without further purification.

*Kinetic measurements*

Polymerization was followed by conventional dilatometry. Reaction rates were rather high for this technique and so special procedures were necessary to eliminate zero time errors consequent on the rapid initiation reactions.

Initiator solutions of potassium tert-butoxide were prepared from stock solutions in sealed thin walled, glass phials. The initiator concentration was estimated by breaking representative phials into water for estimation by titration with standard acid. Suitable glass phials of initiator solution were carefully placed into ordinary Pyrex test tubes having a sharp glass 'spike' protruding from the base inwards. Calibrated capillary stems were then glass welded to the test tube and the complete dilatometer filled with the requisite solvent-monomer mixture by distillation under high vacuum. When the dilatometer was filled, sealed and removed from the vacuum line, it was allowed to reach temperature equilibrium in a suitable constant temperature bath. The reaction was started by vibrating the dilatometer stem with a Vibro stirrer which after a few seconds vibration ruptured the glass phial containing the initiator against the inverted spike, whereupon the vibration was continued for a further short period so as to improve mixing.

Polymerizations were allowed to go to completion after which the polyethylene oxide was recovered by precipitation into cold ether.

*Molecular weights*

Intrinsic viscosities,  $[\eta]$ , were measured in water at 30°C and molecular weights were estimated from the expression<sup>13</sup>

$$[\eta] = 1.25 \times 10^{-4} M^{0.78}$$

## RESULTS

The polymerization of ethylene oxide in DMSO was studied at 25°C and 50°C and the results are shown in *Tables 1* and *2*. Although initial rates showed a linear dependence in both [potassium tert-butoxide] and [ethylene oxide] each kinetic run (at 25°C) gave values of  $\{R_p/[M]_t\}$  which fell steadily with time to a final constant value (see *Figure 1*). This decay was not observed at 50°C and even at 25°C the decay was eliminated by adding 1,2-dimethoxy ethane to the reaction mixture (*Figure 1*).

Physically it was observed that runs at 25°C were accompanied by increasing light scatter by the reaction mixtures and eventually the polymer precipitated. At 50°C apparently the polymer remained soluble throughout.

## DISCUSSION

Polymerization of ethylene oxide in DMSO occurs readily using solutions of potassium tert-butoxide as initiator. Initial reaction rates were given by the expression

$$-d[M]/dt = R_p = k_p [M] [K^+ OBU^-]$$

where  $[M]$  represents the initial concentration of ethylene oxide. Molecular weights of the polymers increased with increasing [monomer] and with decreasing  $[K^+ OBU^-]$ . At very low conversion, when the systems were truly homogeneous, it is likely that the degrees of polymerization approximate to

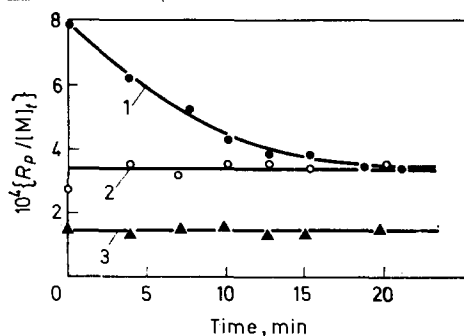
Table 1. Polymerization of ethylene oxide by potassium tert-butoxide in dimethyl sulphoxide at 25°C

| Concentration, mole l <sup>-1</sup> | Initial rates<br>(10 <sup>3</sup> × R <sub>p</sub> )<br>mole l <sup>-1</sup><br>sec <sup>-1</sup> | Initial rate<br>coefficient<br>(10 <sup>3</sup> × k <sub>p</sub> )<br>l. mole <sup>-1</sup><br>sec <sup>-1</sup> | Molecular weights <sup>13</sup>  | % yield |     |
|-------------------------------------|---|--|--|---------|-----|
| Monomer                             | 10 <sup>3</sup> ×<br>Initiator  |  |  |         |     |
| 5.50                                | 12.2  | 8.35   | 12.4   | 11 480  | 89  |
| 4.25                                | 12.2  | 6.20   | 12.0   | 8 510   | 75  |
| 3.22                                | 11.6  | 2.32   | 6.2  | 8 700   | 89  |
| 2.55                                | 12.1  | 2.64   | 8.6  | 7 240   | 66  |
| 1.70                                | 12.2  | 1.36   | 6.6  | 6 630   | 100 |
| 0.84                                | 12.6  | 0.91   | 8.0  | 4 320   | 21  |
| 4.23                                | 15.30   | 7.55   | 11.7   | 8 130   | 85  |
| 4.38                                | 9.34  | 4.48   | 11.0   | 14 130  | 85  |
| 4.08                                | 5.66  | 3.19   | 13.7   | 18 840  | 83  |
| 3.95                                | 5.27  | 2.06   | 9.9  | 13 120  | 74  |
| 4.31                                | 2.19  | 1.22   | 12.8   | 33 100  | 77  |
| 4.06                                | 1.88  | 0.48   | 6.3  | 22 400  | 86  |
| 4.31                                | 0.48  | 0.26   | 12.6   | 45 000  | 76  |
| 1.73                                | 12.4  | 0.24   | 1.1*   | 6 500   | 100 |
| 1.58                                | 7.75  | 0.20   | 1.6 (containing 3.78 × 10 <sup>-2</sup> mole l <sup>-1</sup> Bu <sup>t</sup> OH) |         |     |
| 1.58                                | 7.75  | 0.42   | 3.4 (containing 1.62 × 10 <sup>-2</sup> mole l <sup>-1</sup> Bu <sup>t</sup> OH) |         |     |

\*Containing dimethoxyethane 20% v/v of the total solution.

Table 2. Polymerization of ethylene oxide by potassium tert-butoxide in dimethyl sulphoxide at 50°C

| Concentration, mole l <sup>-1</sup> | Initial rates<br>(10 <sup>3</sup> × R <sub>p</sub> )<br>mole l <sup>-1</sup><br>sec <sup>-1</sup> | Initial rate<br>coefficient<br>(10 <sup>3</sup> × k <sub>p</sub> )<br>l. mole <sup>-1</sup><br>sec <sup>-1</sup> | Molecular weights <sup>13</sup> | % yield |    |
|-------------------------------------|---|--|---------------------------------|---------|----|
| Monomer                             | 10 <sup>3</sup> ×<br>Initiator  |  |                                 |         |    |
| 3.14                                | 9.61  | 6.84   | 23                              | 10 350  | 58 |
| 3.43                                | 7.81  | 6.51   | 24                              | 15 850  | 69 |
| 3.40                                | 5.07  | 2.74   | 16                              | 20 400  | 90 |
| 3.40                                | 2.40  | 1.35   | 17                              | 23 130  | 74 |
| 3.45                                | 1.36  | 0.99   | 21                              | 30 900  | 70 |
| 4.81                                | 7.30  | 7.50   | 22                              | 26 300  | 63 |
| 2.42                                | 7.60  | 5.00   | 27                              | 12 300  | 86 |
| 1.54                                | 7.90  | 3.65   | 30                              | 8 610   | 80 |
| 0.82                                | 7.70  | 2.29   | 36                              | 5 930   | 55 |

Figure 1—Values of  $\{R_p/[M]_t\}$  versus time. Curve 1: monomer concentration 1.70 mole l<sup>-1</sup>, initiator concentration 12.2 × 10<sup>-3</sup> mole l<sup>-1</sup>, temperature 25°C and respectively for curve 2: 1.73, 12.4 × 10<sup>-3</sup>, 25°C, in presence of 20% v/v dimethoxy ethane; curve 3: 1.54, 7.90 × 10<sup>-3</sup>, 50°C

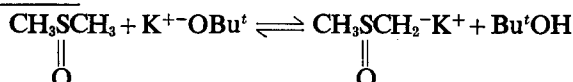
the ratio [monomer used]/[catalyst] but difficulties encountered in recovering all the polymer made it impossible to test this prediction adequately.

Development of micelles and eventual precipitation of polymer was evident from a physical examination of the systems during polymerization, and from the fall in values of  $(R_p/[M])_t$  with time. This effect was most marked at 25°C and was readily relieved either by raising the temperature to 50°C or by addition of 20 vol. % 1,2-dimethoxy ethane—a good solvent for polyethylene oxide (*Figure 1*). DMSO undergoes a phase transition between 35–45°C and clearly becomes a much better solvent for polyethylene oxide above this transition temperature<sup>4</sup>.

*Table 1* also shows that small amounts of added tert-butanol have a pronounced effect on the rate of propagation. Chemical analysis of the lower molecular weight polymers established that sulphur was present in low concentration (< 0.4 per cent) and this would arise from initiation and transfer reactions involving DMSO. Experimentally the sulphur analysis was subject to large errors and hence it is not practicable to attempt correlation between sulphur content and degree of polymerization.

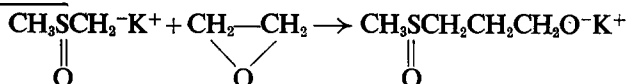
The reactions involved may be summarized as follows:

1. Pre-initiation



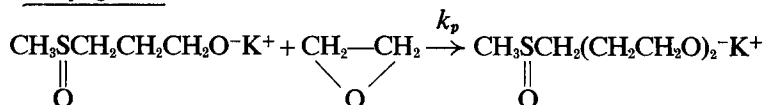
The equilibrium constant for this reaction is  $1.5 \pm 0.5 \times 10^{-7}$ , and the equilibrium is quickly established<sup>5</sup>.

2. Initiation



This reaction is assumed to be fast compared with propagation\*.

3. Propagation



followed by successive monomer additions which are assumed to be kinetically indistinguishable and have the same rate constant  $k_p$ :

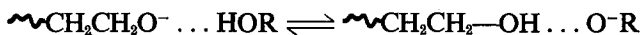
$$\text{at } 25^\circ\text{C, } k_p = 0.10 \pm 0.03 \text{ l. mole}^{-1} \text{ sec}^{-1}$$

$$\text{at } 50^\circ\text{C, } k_p = 0.25 \pm 0.08 \text{ l. mole}^{-1} \text{ sec}^{-1}$$

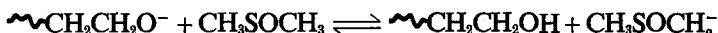
According to this reaction sequence there would be one molecule of <sup>t</sup>BuOH formed for each initiating dimethyl ion. Alcohols in DMSO are known to solvate alkoxide ions strongly via hydrogen bonding and therefore each propagating primary alkoxide ion will be associated with at least one alcohol

\*Even though the dimethyl ion is present in such low concentration, previous work<sup>4</sup> involving addition to benzophenone shows that it is orders of magnitude more reactive than the tert-butoxide ion.

molecule. Initially this would be tert-butanol, formed in the initiation reaction but proton transfer between alcohol and alkoxide ion will be rapid and the end result will be random growth of two polymer molecules per anionic unit, e.g.



Transfer to DMSO is also possible, i.e.



but the molecular weight data show that this reaction is not very important.

In DMSO the propagating potassium alkoxide ion pair is completely dissociated<sup>7</sup> and as a consequence the propagation reaction is very fast. It is interesting to compare the present value of  $k_p$  at 25°C with that determined by Gee, Higginson and Merrall<sup>9</sup> for the polymerization of ethylene oxide by free ions in methanol-dioxan mixture (approximately  $10^{-4}$  l. mole<sup>-1</sup> sec<sup>-1</sup> at 30°C).

At 25°C in DMSO the transition state parameters for polymerization of ethylene oxide are  $\Delta H^\ddagger = 6.4$  kcal mole<sup>-1</sup>,  $\Delta S^\ddagger = -41$  cal mole<sup>-1</sup> deg<sup>-1</sup>. Clearly the high values of  $k_p$  observed are a consequence of the low value of  $\Delta H^\ddagger$  (cf.  $\Delta H^\ddagger$  for propagation in methanol-dioxan<sup>9</sup> is 17.2 kcal mole<sup>-1</sup>).

Overall DMSO provides a medium for polymerization in which the propagating alkoxide is comparatively unsolvated whereas the transition state for propagation (charge dispersed) is highly solvated<sup>3</sup>. This has the effect of lowering  $\Delta H^\ddagger$  and increasing  $\Delta S^\ddagger$ . Introduction of hydrogen bonding substrates such as alcohols (or water) would destroy the favourable solvation characteristics described above.

Recently Price and his collaborators<sup>12</sup> have reported values of rates of polymerization for epoxides in DMSO which are substantially less than those reported here. Furthermore these lower rates were obtained using *higher* initiator concentrations than used here and it is likely that the large discrepancies arise either from heterogeneity of initiator phase in the work of Price *et al.* or perhaps the presence of hydroxylic impurities—the latter now shown to have a marked effect on reaction rates.

Donnan Laboratories,  
University of Liverpool

(Received February 1969)

#### REFERENCES

- CRAM, D. J. *Fundamentals of Carbanion Chemistry*. Academic Press: New York, 1965
- CRAM, D. J., RICKBORN, B. and KNOX, G. R. *J. Amer. chem. Soc.* 1960, **82**, 6412
- PARKER, A. J. *Quart. Rev. chem. Soc., Lond.* 1962, **16**, 163  
PARKER, A. J. *Advanc. Phys. Org. Chemistry* (Ed. V. Gold), **5**, p 173, Academic Press: London, 1967
- MARTIN, D., WEISE, A. and MICLAS, H. J. *Angew. Chem. (Internat. Ed.)*, 1967, **6**, 318  
SCHÖFER, H. L. and SCHAFFERNICHT, W. *Angew. Chem.* 1960, **72**, 618
- LEDWITH, A. and MCFARLANE, N. R. *Proc. chem. Soc.* 1964, 108
- PRICE, G. G. and WHITING, M. C. *Chem. & Ind.* 1963, 775  
COREY, E. J. and CHAYKOVSKY, M. *J. Amer. chem. Soc.* 1962, **84**, 866

## ANIONIC POLYMERIZATION OF ETHYLENE OXIDE

---

- <sup>7</sup> STEINER, E. C. *Polymer Preprints*, American Chemical Society Meeting, Atlantic City, 1968, Vol. IX, No. 2, p 1135
- <sup>8</sup> GAYLORD, N. G. *Polyethers*, Part I. Interscience: New York, 1963  
FURUKAWA, J. and SAEGUSA, T. *Polymerization of Aldehydes and Oxides*. Interscience: New York, 1963  
LEDWITH, A. and FITZSIMMONDS, C. *Polymer Chemistry of Synthetic Elastomers*, p 380. Edited by J. P. KENNEDY and E. G. M. TÖRNQVIST. Interscience: New York, 1968
- <sup>9</sup> GEE, G., HIGGINSON, W. C. E., LEVESLEY, P. and TAYLOR, K. J. *J. chem. Soc.* **1959**, 1338  
GEE, G., HIGGINSON, W. C. E. and MERRALL, G. T. *J. chem. Soc.* **1959**, 1345  
GEE, G., HIGGINSON, W. C. E. and JACKSON, B. *Polymer, Lond.* 1962, **3**, 231
- <sup>10</sup> BAWN, C. E. H., LEDWITH, A. and MCFARLANE, N. R. *Polymer, Lond.* 1967, **8**, 484
- <sup>11</sup> MULVANEY, J. E. and MARKHAM, R. L. *J. Polym. Sci. B*, 1966, **4**, 343  
MOLAN, G. E. and MASON, J. E. *J. Polym. Sci. A.1*, 1966, **4**, 2336  
TROSSARELLI, L., PRIOLA, A., GUAITA, M. and SAINI, G. Reprint No. P. 578, IUPAC, High Polymer Symposium, Prague, 1965
- <sup>12</sup> PRICE, C. C. and CARMELITE, D. D. *J. Amer. chem. Soc.* 1966, **88**, 4039  
PRICE, C. C. and SPECTOR, R. *J. Amer. chem. Soc.* 1966, **88**, 4171
- <sup>13</sup> BAILEY Jr, F. E., KUCERA, T. L. and IMHOFF, L. G. *J. Polym. Sci.* 1958, **32**, 517